

# Enriched Methane Production Technologies

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## 1. Theme description

The Enriched Methane (EM) is a blend composed by Hydrogen and Methane which can be fed, if the H<sub>2</sub> content is lower than 30% vol., into conventional natural gas internal combustion engines with a series of benefits in terms of [\[1\]](#) [\[2\]](#), [\[3\]](#), [\[4\]](#) :

- improvement of engine energy efficiency;
- reduction of CO<sub>2</sub>, CO, unburned hydrocarbons emissions.

The EM can be distributed in the low-medium natural gas grid (if the hydrogen composition is lower than 20% vol. [\[5\]](#) ) and stored by using conventional methane storage system, thus its application being competitive using available and low cost infrastructures. Moreover, since hydrogen has the highest mass lower heating value (kJ/kg), the blend's heating value is greater than those of the methane itself, thus enriching the energy contents.

Basically, if H<sub>2</sub> is produced by exploiting a renewable energy source (solar, wind, biomass), the EM is a sort of a hybrid energy vector (fossil + renewable) with a immediate and competitive potentiality to be applied and a reduced environmental impact due to the strong reduction of CO<sub>2</sub> emissions (up to 11% wt. if a blend of 30% vol H<sub>2</sub> is burned).

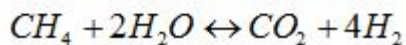
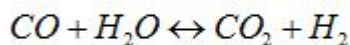
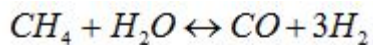
In the present article, the main routes to produce EM blends

are investigated both from fossil fuel and from renewable energies. Then, some applications implemented worldwide are presented.

## 2. Production Processes

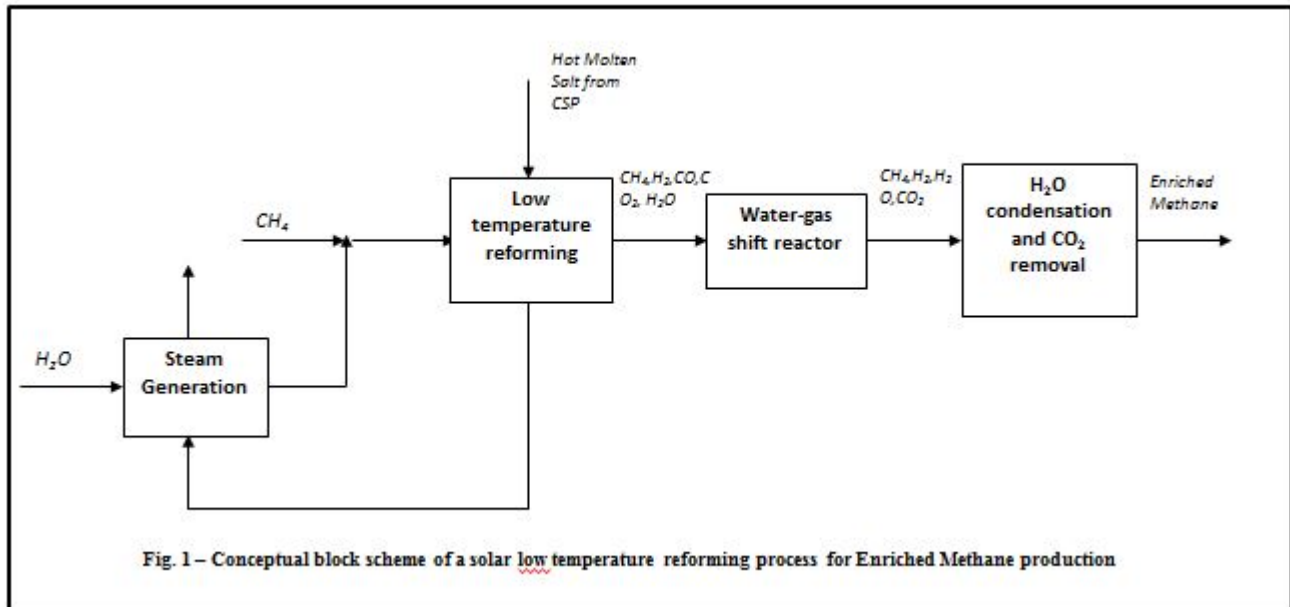
### *2.1 Enriched Methane production from Fossil Fuels*

Natural gas steam reforming is the most used process for the massive production of hydrogen. The process is composed by the following reactions:



and it is strongly endothermic, thus requiring high temperature to achieve high conversion of methane (90% at 850-950°C). In the conventional process, the reactions occur in tubular catalytic reactors placed inside furnace where a share of natural gas (30% approx) is burned to supply the reactions heat duty. But, if a EM stream has to be produced, much lower methane conversion (< 20%) and, consequently, lower operating temperatures (450-500°C) are required to reach the hydrogen content specifics. The main consequence is that the lower thermal level can be targeted concentrating solar radiation by well-know technologies as the Concentrating Solar Power (CSP) developed by ENEA, able to heat up a molten salt stream up to 550°C, reaching a thermal level suitable for the process requirements [\[6\]](#). By this way, the hydrogen is produced exploiting a renewable source, improving the environmental footprint. The following figure shows a conceptual block scheme of the technology: after the low temperature reforming, a water gas shift reactor is installed

to allow the conversion of CO into  $H_2$  and  $CO_2$ ; then the unreacted steam water is removed by condensation and the  $CO_2$  by an ammine-based absorption, while the EM stream is sent to the application.



A variation of the process is the Partial Oxidation Methane Reforming, where the heat duty is supplied thanks to the combustion of a share of input methane directly inside the adiabatic reactor. By this way, the energy needed to produce the hydrogen is fed by a fossil source.

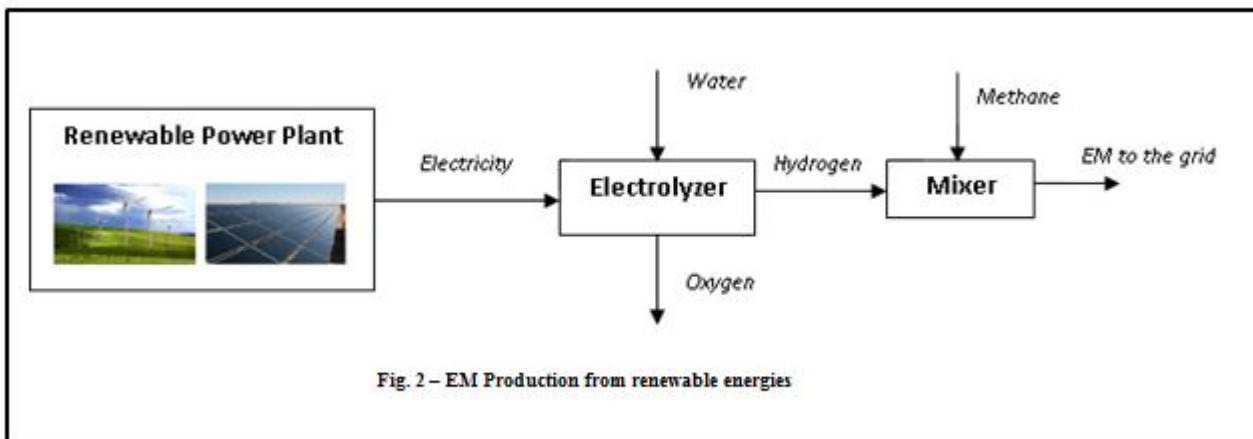
Another process is the coal gasification, able to produce syngas (a mixture of methane, carbon monoxide, hydrogen, carbon dioxide and water vapor) from coal and water, air and/or oxygen. After the gasification reactor, a proper purification system allows to obtain a EM stream with the desired  $H_2$  composition.

## ***2.2 Enriched Methane production from Renewable Electricity***

Hydrogen can be produced from electricity by means of electrolyzers [\[71\]](#), which are able to dissociate the water molecule into hydrogen and oxygen. The electricity can be

produced by renewable power plants as solar photovoltaic, wind farms, hydroelectric plants, etc., so that the hydrogen produced is completely CO<sub>2</sub>-free. Then, mixing the hydrogen with a methane stream, the EM blend is obtained and can be distributed by means of the natural gas grid. The following figure shows the renewable EM plant configuration.

By this architecture, it is possible to convert renewable electricity surplus into a high-added value product as EM, mitigating the intermittent nature of the renewable energy and avoiding overloading of the electricity network.



## ***2.3 Enriched Methane production from Biologic Processes***

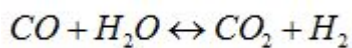
The biological hydrogen production by photosynthetic bacteria, algae or fermentative microorganism appears to be a promising alternative to produce EM.

In anaerobic digestion process different microorganisms are involved to produce methane from complex biomass (as food wastes, organic fraction of municipal solid waste, agro-industrial waste, algae, etc.) through four steps: hydrolysis, acidogenesis, acetogenesis and methanogenesis [\[8\]](#).

To produce EM, a two-phase processes has to be implemented, by which an appropriate separation of acidogenic and methanogenic

phases allows to convert the complex organic material into hydrogen, carbon dioxide and volatile fatty acids during the first stage, and then a conversion of these biodegradable compounds into methane and carbon dioxide during the methanogenic stage.

Moreover, processes able to convert a biomass (solid or liquid) into syngas ( $\text{CO} + \text{H}_2$ ), as the gasification, can be applied to produce EM. The gasificator can be coupled with a water gas shift reactor where the following reaction is promoted:



producing hydrogen from carbon monoxide. Then, the hydrogen is purified from  $\text{CO}_2$  and the trace of  $\text{CO}$ , mixed with methane and used.

### 3.Applications

Some EM pilot applications have been implemented worldwide. Among them, the following have to be cited:

- **Mhybus Project** [\[9\]](#): a EM-fuelled bus has been developed and circulated on urban roads in the city of Ravenna. The bus ran for more than 45,000 km on a normal service line, with an average of 212 km per day and more than 10.000 passengers on board, attesting the EM application feasibility. A yearly saving of 419 € for each bus using EM instead of natural gas has been quantified.



- **ALT-HY-TUDE Project** tested two buses fuelled by Hythane® (a mixture of 20%vol H<sub>2</sub> and 80%vol CH<sub>4</sub>) in the city of Dunkerque [\[10\]](#). The project has been lead by the Research Division of Gaz de France. The hydrogen is produced by an electrolyzer in a specific filling station and then it is mixed with hydrogen to be fuelled in the bus with a natural gas conventional storage system.



- **METISOL** was a research project, funded by a consortium lead by Centro Ricerche FIAT (CRF), focused on the development of a EM production plant coupled with a concentrating solar power plant (CSP). Hydrogen is



produced a low temperature steam reformer (500°C) and a pilot plant able to generate 1 Nm<sup>3</sup>/h of EM (30% vol. H<sub>2</sub>) has been installed and tested in ENEA laboratories [\[11\]](#).



- **Malmö Hydrogen and CNG/Hydrogen filling station.** A hydrogen production plant, connected with a EM filling station and composed by an electrolyzer, has been located in Malmö (Sweden) [\[12\]](#). The filling station is owned and operated by E.ON Gas Sverige AB. The EM produced (8% vol H<sub>2</sub>) feeds two local buses, which have been tested for more than 3 years.



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[1] Bauer CG, Forest TW. Effect of hydrogen addition on the performance of methane-fueled vehicles. Part I: effect of S.I. engine performance. International Journal of Hydrogen Energy 2001;26:55–70.

[2] Bauer CG, Forest TW. Effect of hydrogen addition on the performance of methane-fueled vehicles. Part II: driven cycle simulations. International Journal of Hydrogen Energy 2001; 26:71–90.

[3] Orhan Akansu S, Dulger Z, Kaharaman N, Veziroglu TN. Internal combustion engines fuelled by natural gas–hydrogen mixtures. International Journal of Hydrogen Energy 2004;29:1527–39.

[4] Ortenzi F, Chiesa M, Scarcelli R, Pede G. Experimental tests of blends of hydrogen and natural gas in light-duty vehicles. International Journal of Hydrogen Energy 2008;33:3225–9.

[5] Haeseldonckx D, D'haeseleer W. The use of natural-gas pipeline infrastructure for hydrogen transport in a changing market structure. International Journal of Hydrogen Energy 2007;32:1381–6.

[6] De Falco M, Giaconia A, Marrelli L, Tarquini P, Grena R, Caputo G. Enriched methane production using solar energy: an assessment of plant performance. International Journal of Hydrogen Energy 2009; 34: 98-109.

[7] <http://www.nrel.gov/docs/fy04osti/36705.pdf>

[8] Cavinato C , Bolzonella D, Fatone F, Cecchi F, Pavana P. Optimization of two-phase thermophilic anaerobic digestion of biowaste for hydrogen and methane production through reject water recirculation. Bioresource Technology 2011;102:8605–8611.

[9] [http://community.aster.it/mhybus/en/mhybus\\_en.htm](http://community.aster.it/mhybus/en/mhybus_en.htm)



[\[10\]](#)

[http://www.althytude.info/fileadmin/user\\_upload/documents/trip tyque.pdf](http://www.althytude.info/fileadmin/user_upload/documents/trip tyque.pdf)

[\[11\]](#)

[http://link.springer.com/chapter/10.1007/978-3-319-22192-2\\_3](http://link.springer.com/chapter/10.1007/978-3-319-22192-2_3)

[\[12\]](#)

<http://www.cder.dz/A2H2/Medias/Download/Proc%20PDF/PARALLEL%20SESSIONS/%5BS26%5D%20 Deployment/13-06-06/339.pdf>